Listing of Claims:

CLAIMS

1. (currently amended) A method for the dilution of dewatered and compressed cellulose pulp that has been consolidated into large pieces, where the dewatered cellulose pulp maintains a first consistency greater than 20%, comprising: fragmenting the cellulose pulp into a finely divided pulp after or in association with dewatering, thus granulating the cellulose pulp through said fragmentation to a particle size with a normal distribution with a maximum size that is less than 40 mm, while fragmenting, maintaining a consistency of the cellulose pulp that is essentially equivalent to the first consistency, feeding the cellulose pulp that has been finely divided through the fragmentation into a freely falling flow, adding dilution fluid under pressure towards the freely falling fragmented pulp through a number of fluid jets arranged in association with the flow of the freely falling fragmented pulp, the amount of dilution fluid added through the fluid jets establishing a second consistency of the cellulose pulp in a medium-consistency range 8-16%, feeding the cellulose pulp at this medium consistency 8-16% onwardly to subsequent treatment stages, a dilution of the freely falling pulp taking place essentially exclusively under an influence of hydrodynamic effect from the addition of the dilution fluid through the fluid jets, and where no mechanical agitation ~~taking~~ takes place between the fragmentation of the cellulose pulp and an underlying surface ~~(LiqLEV)~~ of the cellulose pulp that has been diluted by the dilution fluid.

2. (original) The method according to claim 1, wherein the fluid jets are arranged around the flow of fragmented pulp formed in the free fall, and are directed principally radially inwards towards the flow.

3. (original) The method according to claim 1, wherein the cellulose pulp at medium consistency is fed onwardly to subsequent treatment stages through pumping.

4. (original) The method according to claim 1 wherein the dilution fluid added is added to a degree of more than 50%, through the fluid jets.

5. (original) The method according to claim 1 wherein the addition of dilution fluid from the fluid jets takes place in a form of pressurized fluid jets that are directed obliquely downwardly in a fall direction of the cellulose pulp.

6. (original) The method according to claim 4, wherein the fluid jets are directed at an angle of 45°±15° relative to a vertical direction and a fall direction of granulate.

7. (withdrawn) A device for the dilution of dewatered cellulose pulp, comprising; shredder screw means for fragmenting pulp to a particle size in an interval of 5-40 millimeters, the shredder screw means having an outlet defined therein, the shredder screw means containing the fragmented pulp, a vertical standpipe connected to the outlet of the shredder screw means, the standpipe carrying a flow of the fragmented pulp flowing under free fall, the standpipe having a distribution chamber defined therein at an upper end of the stand pipe, the distribution chamber arranged concentrically around the standpipe, at least four nozzles arranged around a circumference of the distribution chamber, the nozzles being oriented inwardly towards a center of the flow to add a dilution fluid under pressure into the stand pipe, the nozzles being disposed above a liquid level of diluted pulp established in the standpipe, a feed arrangement disposed at a bottom of the standpipe for feeding the pulp to subsequent treatment stages, a pump disposed at the bottom of the standpipe and in operative engagement with the feed arrangement, and the standpipe having no mechanical agitator disposed above the liquid level.

8. (withdrawn) The device according to claim 7 wherein the device has the pump connected to the stand pipe at a lower part thereof close to the bottom of the stand pipe under the liquid level.

9. (withdrawn – currently amended) The device according to claim 7 wherein the nozzles are arranged around a periphery of the stand pipe, where a distance between ~~neighbouring~~ neighboring nozzles is less than 50-300 mm.

10. (withdrawn) The device according to claim 9 wherein each nozzle is directed at an angle relative to a direction of free fall of the fragmented pulp of 45°±15°.

11. (withdrawn – currently amended) The device according to claim 10 wherein all nozzles are connected to a common distribution chamber for dilution fluid, and the distribution chamber is pressurized through a pressure-raising device.

12. (withdrawn) The device according to claim 7 wherein the nozzles are oriented obliquely downwardly.